

Transport phenomena

CO_2
 O_2

Transport of matter

fog

water + nutrients

rain

Transport phenomena

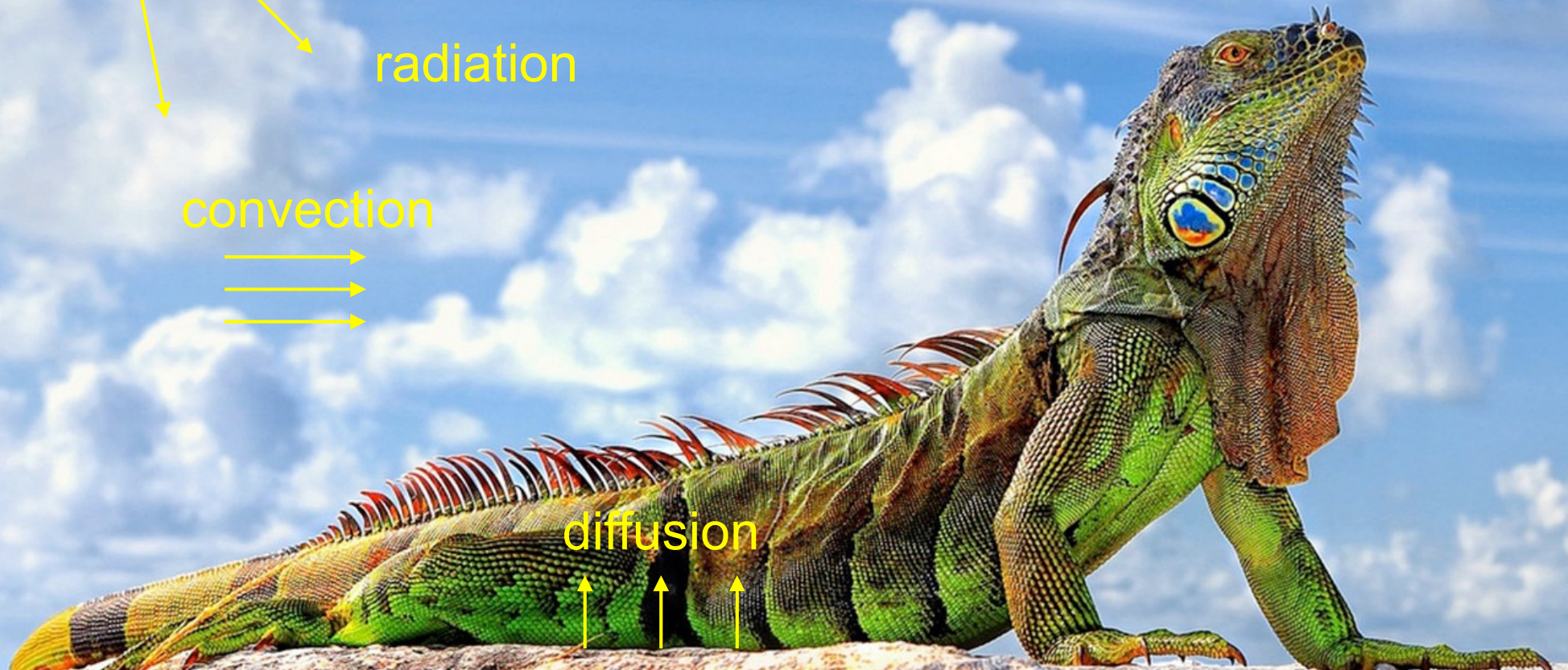


Transport of heat
radiation

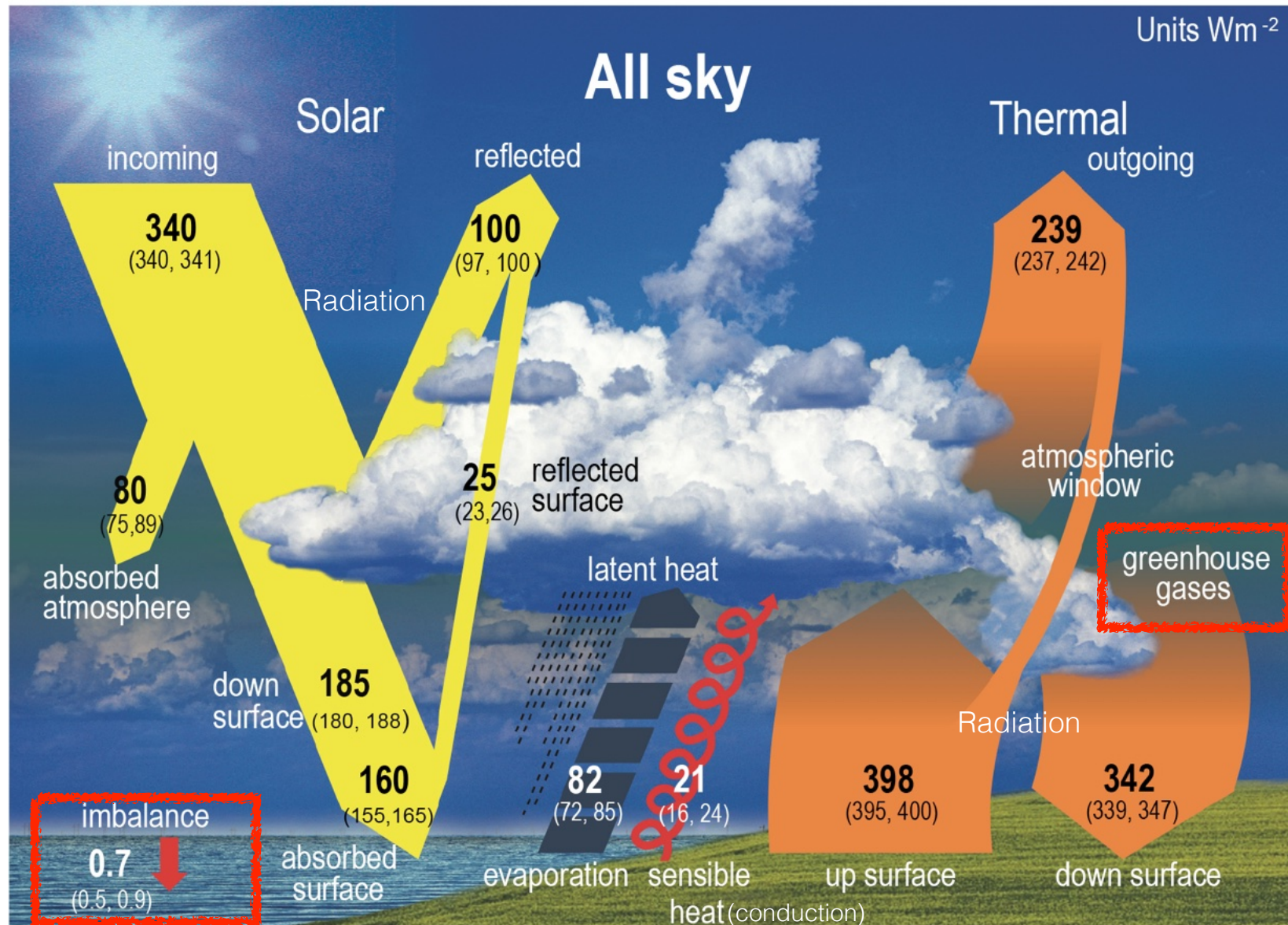
convection



diffusion



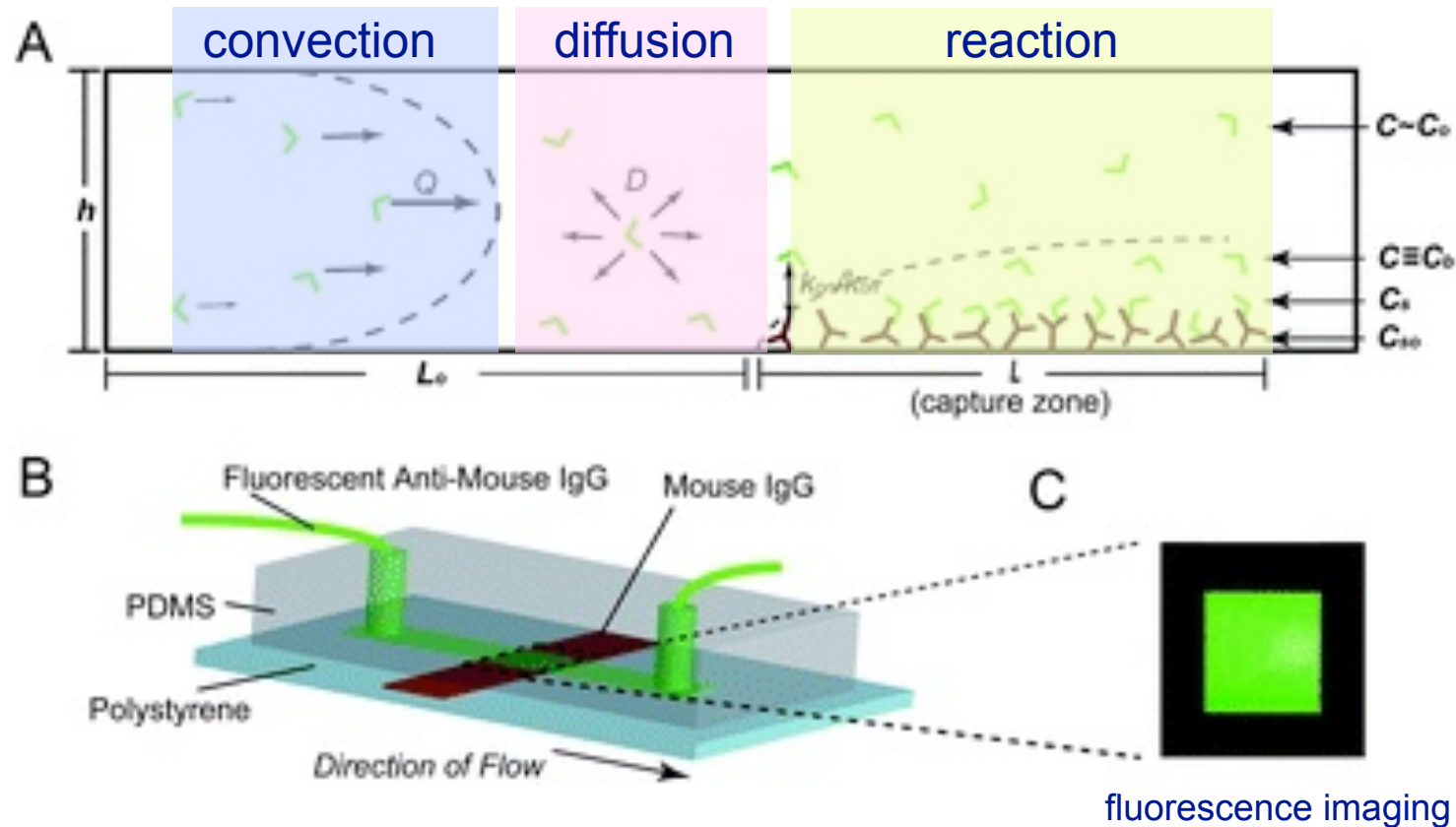
Earth thermal budget



0.2% of global exchanges

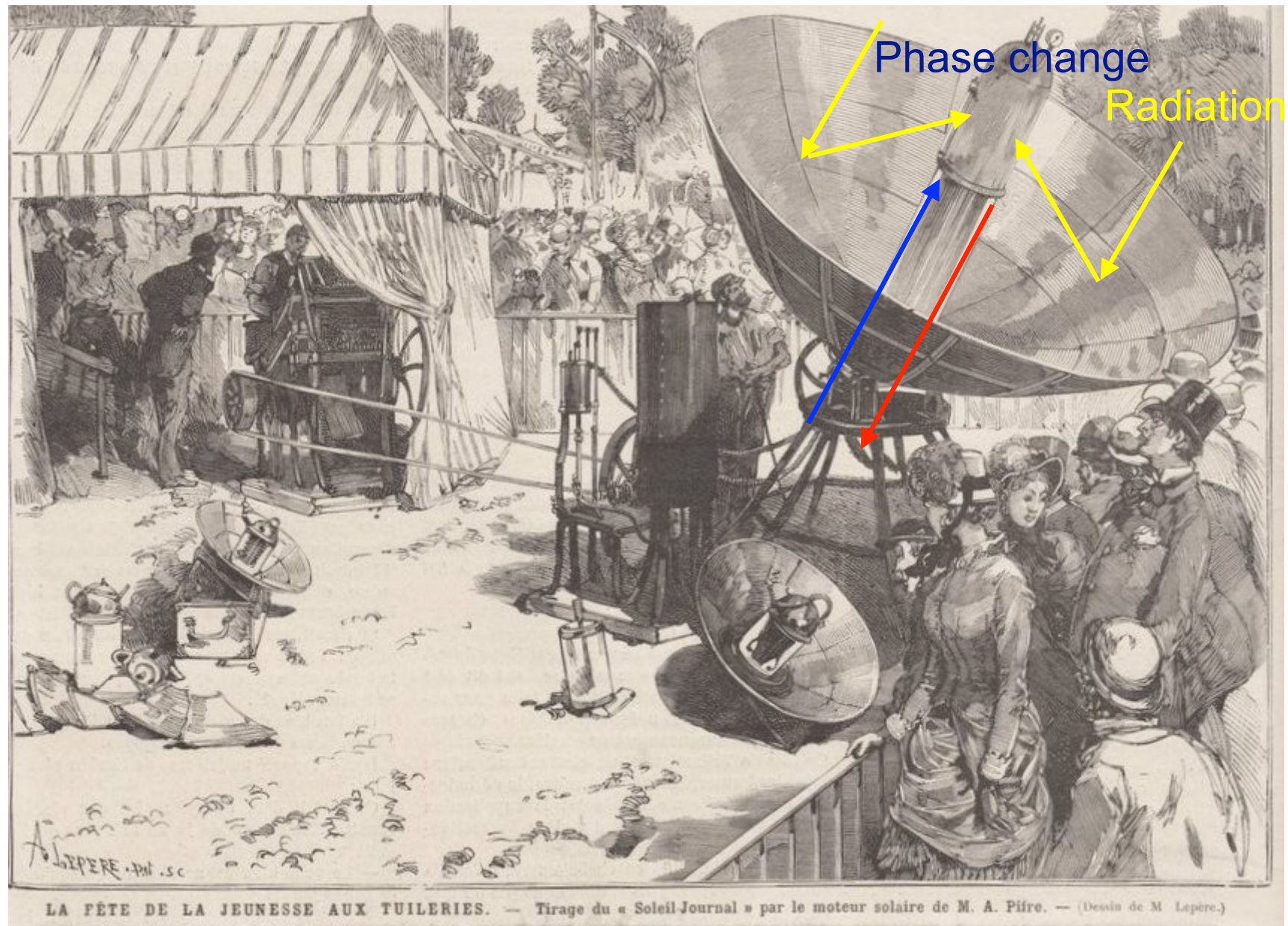
IPCC technical report

Engineering at small scale : designing a microchip ?



→ course on Microfluidics: Nicolas Bremond

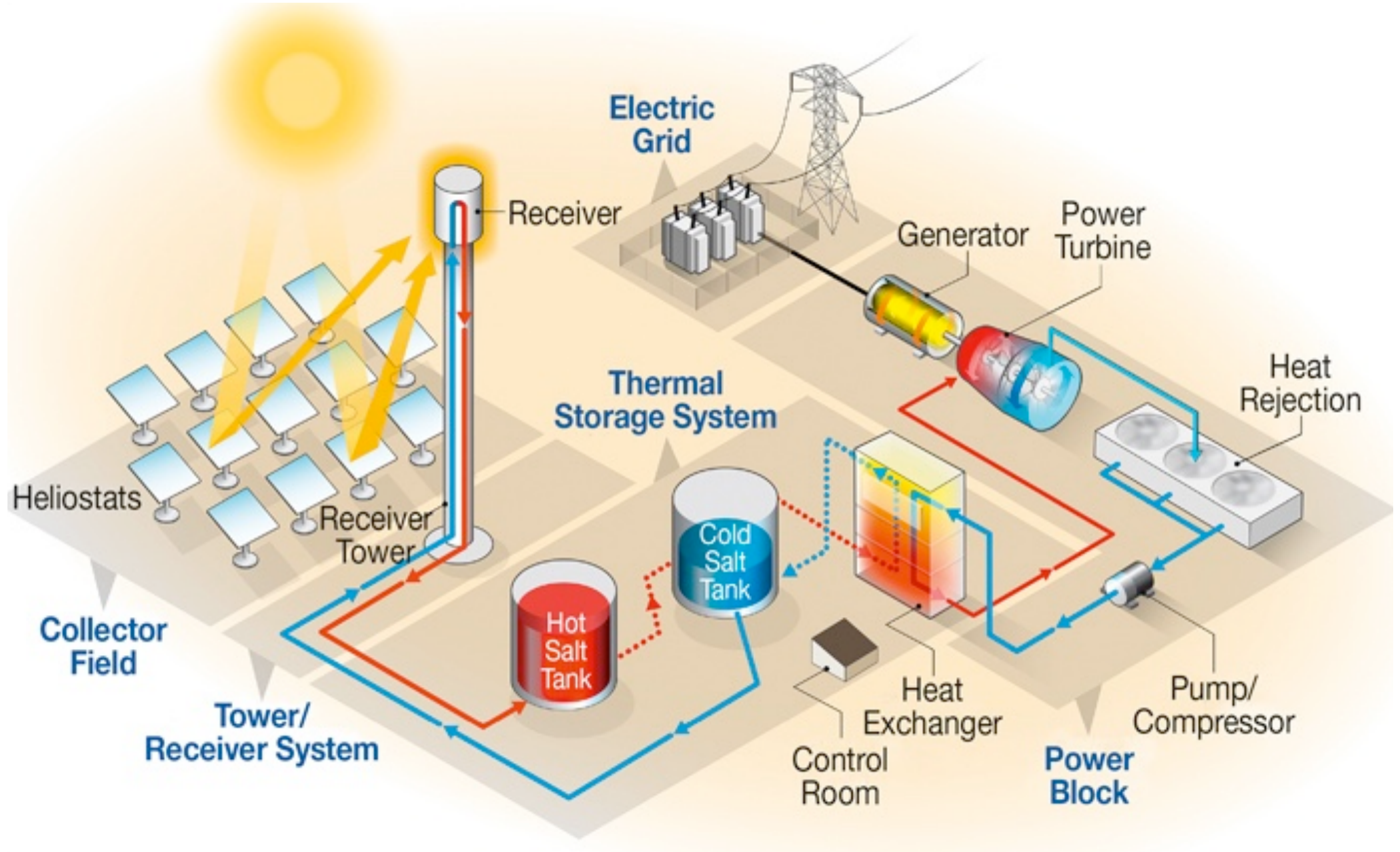
Engineering at large scale : a solar power plant



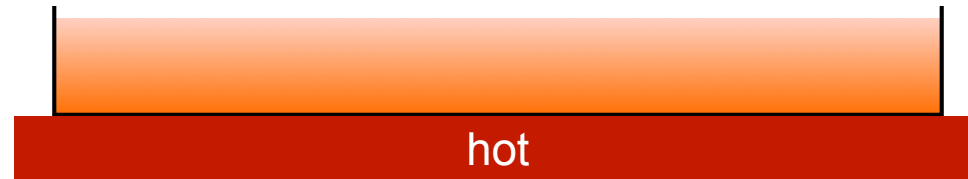
Augustin Mouchot, a pioneer

Le Monde Illustré (1882)

Engineering at large scale : a solar power plant



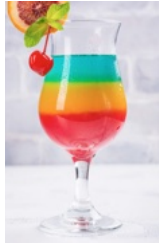
And some instabilities



<https://youtu.be/nQUH9nGTZTY>

→ course on Instabilities: Laurent Duchemin

Outline: learning from problems



1. Diffusion: mixing time of a cocktail, Adding convection
2. Simple transport problems #1: measuring a diffusion coefficient
3. Simple transport problems #2: contact temperature, melting time of an ice cube, temperature inside a cave
4. Forced convection & boundary layers: wind powered fridge
5. Natural convection: designing an igloo
6. Convection-induced instabilities: convection cells
7. Radiative transfer
8. Thermal imaging
9. Recap: Solidifying droplet, Penguins feet.

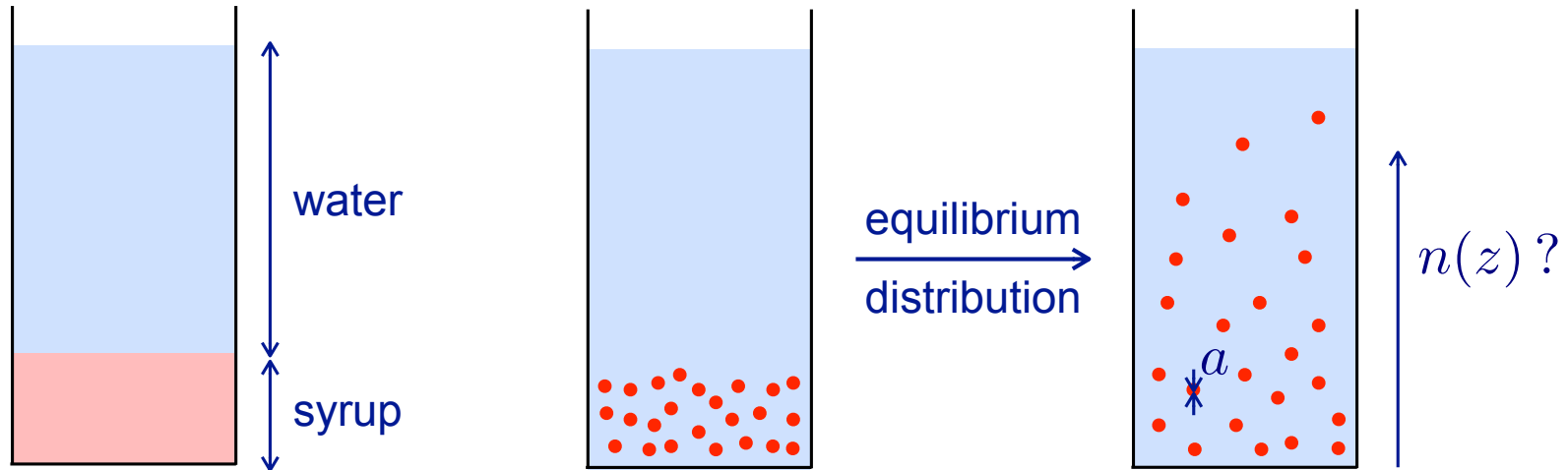
Diffusion in a layered cocktail



Is the configuration stable ?

How long will it take to vanish ?

Diffusion in a layered cocktail



Statistical Physics

$$\mathcal{U}_p = \frac{4}{3}\pi a^3 \Delta\rho g z \quad n(z) = n_0 \exp\left(-\frac{\mathcal{U}_p}{k_B T}\right) = n_0 \exp(-z/\lambda)$$

with

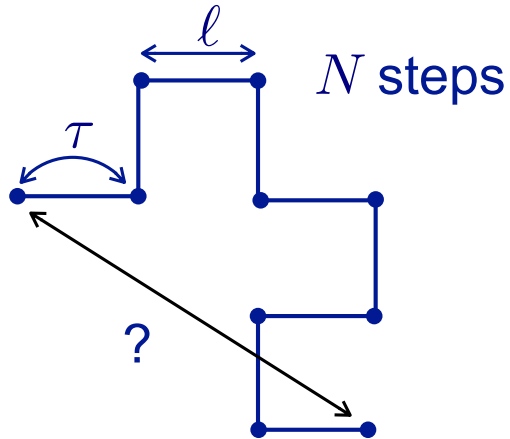
$$\lambda = \frac{k_B T}{\frac{4}{3}\pi a^3 \Delta\rho g}$$

numerical estimate:

$$k_B T = 4 \cdot 10^{-21} \text{ J} \quad \Delta\rho \sim 600 \text{ kg/m}^3 \quad a \sim 10^{-9} \text{ m} \quad \Rightarrow \quad \lambda \sim 100 \text{ m} !$$

Random walks

Very simplified model



$$x = \sum^N \ell \delta_i \quad \delta_i = \pm 1 \Rightarrow \langle x \rangle = 0$$

$$x^2 = \ell^2 \left(\sum^N \delta_i^2 + \sum^{N,N} \delta_i \delta_j \right)$$

$$\langle \delta_i \delta_j \rangle = 0$$

$$\langle x^2 \rangle = N \ell^2$$

$$t = N \tau \Rightarrow \langle x^2 \rangle = \frac{\ell^2}{\tau} t$$

Dissipation for each step

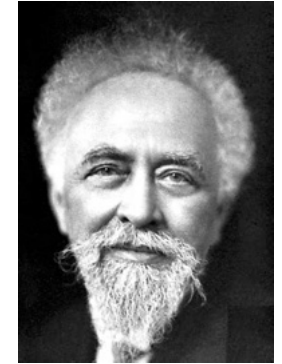
viscous drag $6\pi\eta a U \ell \sim k_B T$ $U \sim \frac{\ell}{\tau} \Rightarrow \frac{\ell^2}{\tau} = D = \frac{k_B T}{6\pi\eta a}$

numerical estimate:

$$k_B T = 4 \cdot 10^{-21} \text{ J} \quad \eta = 10^{-3} \text{ Pa.s} \quad a \sim 10^{-9} \text{ m} \quad D \sim 2 \cdot 10^{-10} \text{ m}^2/\text{s}$$

homogenization over 10 cm: $5 \cdot 10^7 \text{ s} \sim 1.5 \text{ year} !$

Jean Perrin



1870-1942

Sedimentation

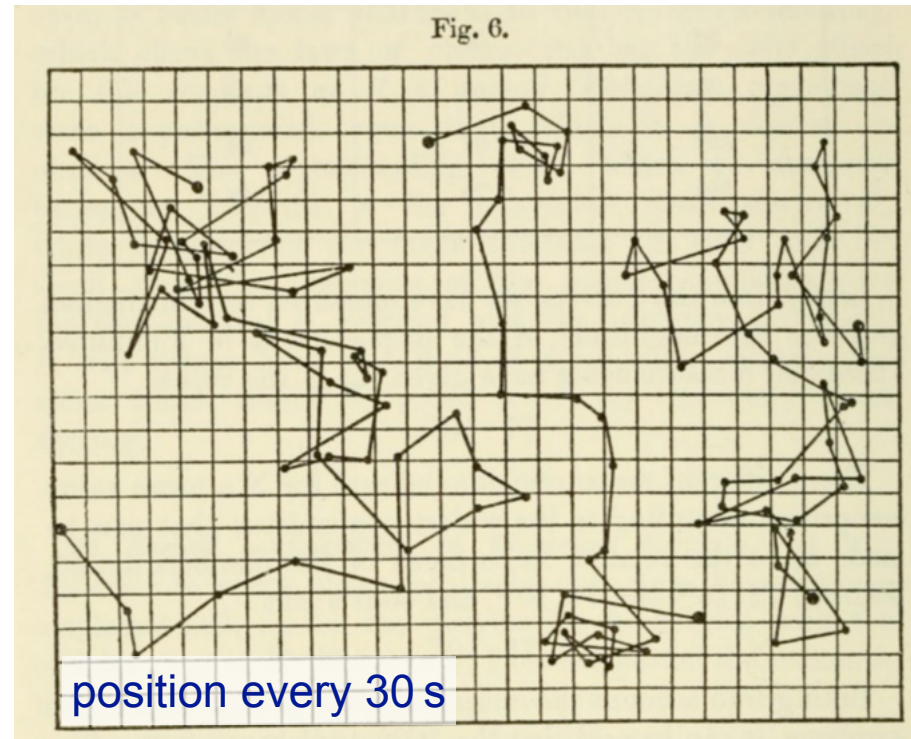


10 μm

resin droplets, $a \sim 0.3 \mu\text{m}$

$$\lambda = \frac{k_B T}{\frac{4}{3} \pi a^3 \Delta \rho g}$$

Diffusion



Perfect gas constant
(already known)

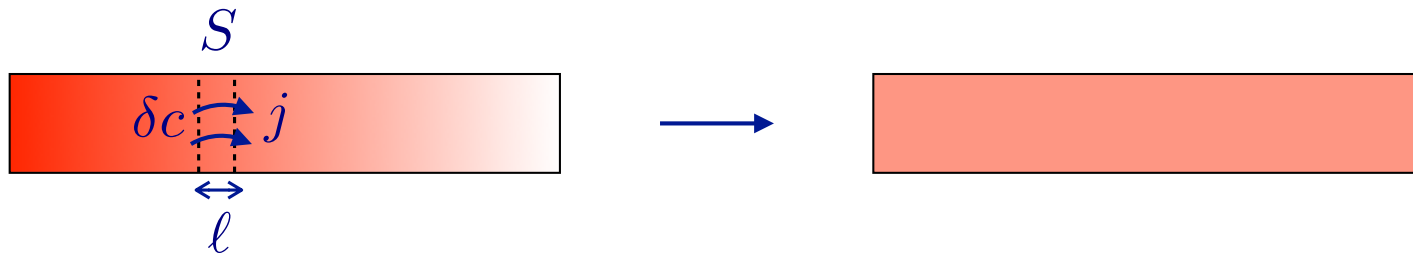
$$D = \frac{k_B T}{6 \pi \eta a}$$

Estimates of $k_B T \Rightarrow \mathcal{N}_A = \frac{R}{k_B}$

Les Atomes (1913)

Fluxes

Fick's law



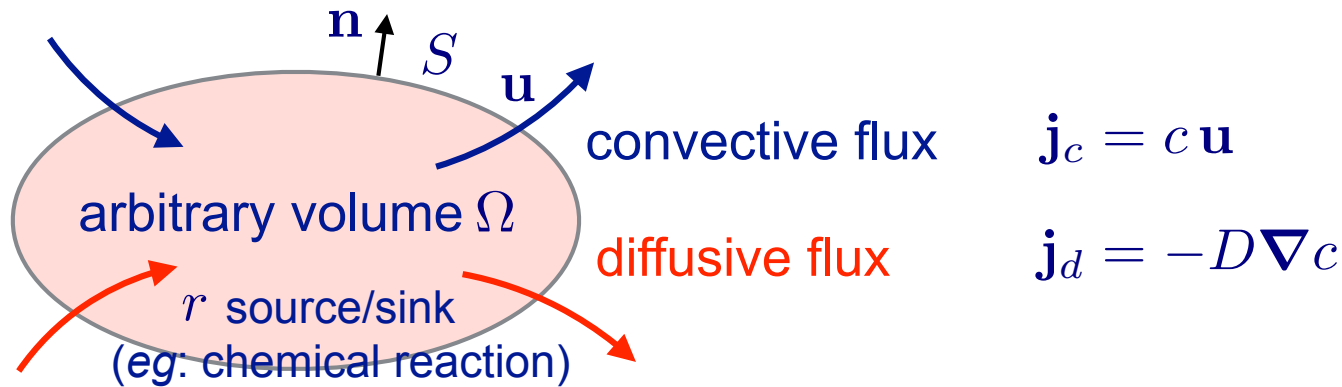
$$S j \tau = S l \delta c \Rightarrow j = \frac{\delta c}{\tau} l = \frac{\delta c}{l} \frac{l^2}{\tau}$$

$$\frac{\delta c}{l} \leftrightarrow -\frac{\partial c}{\partial x} \Rightarrow j = -\frac{l^2}{\tau} \frac{\partial c}{\partial x} = -D \frac{\partial c}{\partial x}$$

Generalization

$$j = -D \nabla c$$

Adding convection



$$\mathbf{j}_c = c \mathbf{u}$$

$$\mathbf{j}_d = -D \nabla c$$

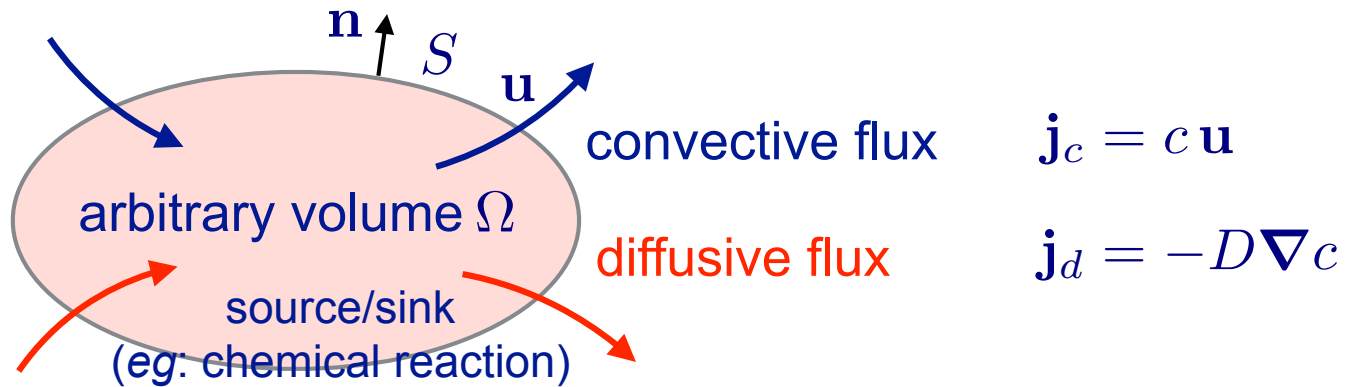
quantity inside the volume (moles, particules, mass): $N = \iiint_{\Omega} c d\Omega$

evolution in time:
$$\frac{dN}{dt} = \iiint_{\Omega} \frac{\partial c}{\partial t} d\Omega = - \iint_S (\mathbf{j}_c + \mathbf{j}_d) \cdot \mathbf{n} dS + \iiint_{\Omega} r d\Omega$$

divergence theorem:
$$\iiint_{\Omega} \frac{\partial c}{\partial t} d\Omega = - \iiint_{\Omega} \nabla \cdot (\mathbf{j}_c + \mathbf{j}_d) d\Omega + \iiint_{\Omega} r d\Omega$$

since Ω is arbitrary:
$$\frac{\partial c}{\partial t} = -\nabla \cdot (\mathbf{j}_c + \mathbf{j}_d) + r$$

Adding convection



$$\frac{\partial c}{\partial t} = -\nabla \cdot (c \mathbf{u}) + \nabla \cdot (D \nabla c) + r$$

$$\frac{\partial c}{\partial t} = -c \cancel{\nabla \cdot \mathbf{u}} - \mathbf{u} \cdot \nabla c + D \Delta c + \cancel{\nabla D \cdot \nabla c} + r$$

incompressible flow

assume D uniform

Diffusion-convection equation

$$\frac{\partial c}{\partial t} + \mathbf{u} \cdot \nabla c = D \Delta c + r$$

+ Navier & Stokes

$$\frac{\partial \mathbf{u}}{\partial t} + (\mathbf{u} \cdot \nabla) \mathbf{u} = \nu \Delta \mathbf{u} - \frac{1}{\rho} \nabla p + \mathbf{g}$$