Hydrodynamics

Class 9

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Rayleigh-Bénard Convection



Rayleigh-Bénard Convection

- **Boussinesq Approximation**
- Calculation and subtraction of the basic state
- Non-dimensionalisation
- **Boundary Conditions**
- Linear stability analysis

Boussinesq Approximation

 μ (viscosity ~ diffusivity of momentum), κ (diffusivity of temperature), ρ (density) constant except in buoyancy force. Valid for $T_0 - T_1$ not too large.

$$\rho(T) = \rho_0 \left[1 - \alpha (T - T_0) \right]$$
$$\nabla \cdot \mathbf{U} = 0$$

Governing equations:

$$\rho_0 \left[\partial_t + (\mathbf{U} \cdot \nabla)\right] \mathbf{U} = \mu \Delta \mathbf{U} - \nabla P - g\rho(T) \hat{\boldsymbol{e}}_z$$
$$\left[\partial_t + (\mathbf{U} \cdot \nabla)\right] T = \kappa \Delta T$$
$$\uparrow \qquad \uparrow \qquad \uparrow$$
advection diffusion buoyancy

Boundary conditions:

$$U = 0$$
 at $z = 0, d$
 $T = T_{0,1}$ at $z = 0, d$

Calculation and subtraction of base state

Conductive solution:
$$(U^*, T^*, P^*)$$

Motionless: $U^* = 0$
uniform temperature gradient: $T^* = T_0 - (T_0 - T_1)\frac{z}{d}$
density: $\rho(T^*) = \rho_0 \left[1 + \alpha(T_0 - T_1)\frac{z}{d}\right]$

Hydrostatic pressure counterbalances buoyancy force:

$$P^* = -g \int dz \ \rho(T^*) \\ = P_0 - g\rho_0 \left[z + \alpha (T_0 - T_1) \frac{z^2}{2d} \right]$$

Write:

$$T = T^* + \hat{T} \quad P = P^* + \hat{P}$$

Buoyancy:

$$\begin{split} \rho(T^* + \hat{T}) &= \rho_0 (1 - \alpha (T^* + \hat{T} - T_0)) \\ &= \rho_0 (1 - \alpha (T^* - T_0)) - \rho_0 \alpha \hat{T} \\ &= \rho(T^*) - \rho_0 \alpha \hat{T} \\ -\nabla P - g\rho(T) \hat{\boldsymbol{e}}_{\boldsymbol{z}} &= -\nabla P^* - g\rho(T^*) - \nabla \hat{P} + g\rho_0 \alpha \hat{T} \hat{\boldsymbol{e}}_{\boldsymbol{z}} \\ &= -\nabla \hat{P} + g\rho_0 \alpha \hat{T} \hat{\boldsymbol{e}}_{\boldsymbol{z}} \end{split}$$

Advection of temperature:

$$(U \cdot \nabla)T = (U \cdot \nabla)T^* + (U \cdot \nabla)\hat{T}$$

= $(U \cdot \nabla) \left(T_0 - (T_0 - T_1)\frac{z}{d}\right) + (U \cdot \nabla)\hat{T}$
= $-\frac{T_0 - T_1}{d}U \cdot \hat{e}_z + (U \cdot \nabla)\hat{T}$

Governing equations:

$$\rho_0 \left[\partial_t + (U \cdot \nabla)\right] U = -\nabla \hat{P} + g \rho_0 \alpha \hat{T} \hat{\boldsymbol{e}}_{\boldsymbol{z}} + \mu \Delta U$$
$$\nabla \cdot U = 0$$
$$\left[\partial_t + (U \cdot \nabla)\right] \hat{T} = \frac{T_0 - T_1}{d} U \cdot \hat{\boldsymbol{e}}_{\boldsymbol{z}} + \kappa \Delta \hat{T}$$

Homogeneous boundary conditions:

$$U = 0$$
 at $z = 0, d$
 $\hat{T} = 0$ at $z = 0, d$

Non-dimensionalization

Scales:

$$z = d\bar{z}, \quad t = \frac{d^2}{\kappa}\bar{t}, \quad U = \frac{\kappa}{d}\bar{U}, \quad \hat{T} = \frac{\mu\kappa}{d^3g\rho_0\alpha}\bar{T}, \quad \hat{P} = \frac{\mu\kappa}{d^2}\bar{P}$$

Equations :

$$\frac{\kappa^2 \rho_0}{d^3} \left[\partial_{\bar{t}} + (\bar{U} \cdot \bar{\nabla}) \right] \bar{U} = -\frac{\mu \kappa}{d^3} \bar{\nabla} \bar{P} + \frac{\mu \kappa}{d^3} \bar{T} \hat{\boldsymbol{e}}_{\boldsymbol{z}} + \frac{\mu \kappa}{d^3} \bar{\Delta} \bar{U}$$
$$\frac{\kappa}{d^2} \bar{\nabla} \cdot \bar{U} = 0$$
$$\frac{\mu \kappa^2}{d^5 g \rho_0 \alpha} \left[\partial_{\bar{t}} + (\bar{U} \cdot \bar{\nabla}) \right] \bar{T} = \frac{\kappa}{d} \frac{T_0 - T_1}{d} \bar{U} \cdot \hat{\boldsymbol{e}}_{\boldsymbol{z}} + \frac{\mu \kappa^2}{d^5 g \rho_0 \alpha} \bar{\Delta} \bar{T}$$

Dividing through, we obtain:

$$\begin{bmatrix} \partial_{\bar{t}} + (\bar{U} \cdot \bar{\nabla}) \end{bmatrix} \bar{U} = \frac{\mu}{\rho_0 \kappa} \begin{bmatrix} -\bar{\nabla}\bar{P} + \bar{T}\hat{e}_z + \bar{\Delta}\bar{U} \end{bmatrix}$$
$$\begin{bmatrix} \partial_{\bar{t}} + (\bar{U} \cdot \bar{\nabla}) \end{bmatrix} \bar{T} = \frac{(T_0 - T_1)d^3g\rho_0\alpha}{\kappa\mu} \bar{U} \cdot \hat{e}_z + \bar{\Delta}\bar{T}$$

Non-dimensional parameters:

the Prandtl number:

 $Pr \equiv \frac{\mu}{\rho_0 \kappa}$ momentum diffusivity / thermal diffusivity

the Rayleigh number:

 $Ra \equiv \frac{(T_0 - T_1)d^3g\rho_0\alpha}{\kappa\mu}$ non-dimensional measure of thermal gradient

Boundary conditions

Horizontal direction: periodicity $2\pi/q$

Vertical direction: at z = 0, 1

 $T = 0|_{z=0,1} \text{ perfectly conducting plates}$ $w = 0|_{z=0,1} \text{ impenetrable plates}$ Rigid boundaries at z = 0, 1:

 $u|_{z=0,1} = v|_{z=0,1} = 0$ zero tangential velocity

Incompressibility

$$\partial_x u + \partial_y v + \partial_z w = 0$$
$$\implies \partial_z w = -(\partial_x u + \partial_y v)$$

 $\begin{aligned} u|_{z=0,1} &= v|_{z=0,1} = 0 \Longrightarrow \quad \partial_x u|_{z=0,1} = \partial_y v|_{z=0,1} = 0 \\ &\implies \quad \partial_z w|_{z=0,1} = 0 \end{aligned}$

Free surfaces at z = 0, 1 to simplify calculations:

$$\begin{bmatrix} \partial_z u + \partial_x w \end{bmatrix}_{z=0,1} = \begin{bmatrix} \partial_z v + \partial_y w \end{bmatrix}_{z=0,1} = 0$$

zero tangential stress

$$\begin{split} w|_{z=0,1} &= 0 \implies \partial_x w|_{z=0,1} = \partial_y w|_{z=0,1} = 0 \\ \implies \partial_z u|_{z=0,1} = \partial_z v|_{z=0,1} = 0 \\ \implies \partial_x \partial_z u|_{z=0,1} = \partial_y \partial_z v|_{z=0,1} = 0 \\ \implies \partial_{zz} w|_{z=0,1} = -\partial_z (\partial_x u + \partial_y v)|_{z=0,1} = 0 \end{split}$$

Not realistic, but allows trigonometric functions $\sin(k\pi z)$

Two-dimensional case



No-penetration boundary condition:

Horizontal flux:
$$0 = w = \partial_x \psi \Longrightarrow \begin{cases} \psi = \psi_1 & \text{at } z = 1\\ \psi = \psi_0 & \text{at } z = 0 \end{cases}$$
$$\int_{z=0}^1 dz \ u(x,z) = -\int_{z=0}^1 dz \ \partial_z \psi(x,z) = -\psi(x,z)]_{z=0}^1 = \psi_0 - \psi_1$$

Arbitrary constant $\implies \psi_0 = 0$ Zero flux $\implies \psi_1 = 0$ Stress-free: $0 = \partial_z u = -\partial_{zz}^2 \psi$ Rigid: $0 = u = \partial_z \psi$ at z = 0, 1



Temperature equation:

$$\partial_t T + \boldsymbol{U} \cdot \boldsymbol{\nabla} T = RaU \cdot \hat{\boldsymbol{e}}_{\boldsymbol{z}} + \Delta T$$

$$U \cdot \nabla T = u \partial_x T + w \partial_z T$$

= $-\partial_z \psi \partial_x T + \partial_x \psi \partial_z T \equiv J[\psi, T]$

 $\partial_t T + J[\psi, T] = Ra \; \partial_x \psi + \Delta T$

Velocity equation

 $\partial_t U + (U \cdot \nabla)U = Pr \left[-\nabla P + T\hat{\boldsymbol{e}}_{\boldsymbol{z}} + \Delta U\right]$ Take $\hat{\boldsymbol{e}}_{\boldsymbol{y}} \cdot \nabla \times$:

$$\hat{\boldsymbol{e}}_{\boldsymbol{y}} \cdot \boldsymbol{\nabla} \times \partial_t U = \hat{\boldsymbol{e}}_{\boldsymbol{y}} \cdot \boldsymbol{\nabla} \times \boldsymbol{\nabla} \times \partial_t \psi \hat{\boldsymbol{e}}_{\boldsymbol{y}} = -\partial_t \Delta \psi$$
$$\hat{\boldsymbol{e}}_{\boldsymbol{y}} \cdot \boldsymbol{\nabla} \times \boldsymbol{\nabla} P = 0$$
$$\hat{\boldsymbol{e}}_{\boldsymbol{y}} \cdot \boldsymbol{\nabla} \times T \hat{\boldsymbol{e}}_{\boldsymbol{z}} = -\partial_x T$$
$$\hat{\boldsymbol{e}}_{\boldsymbol{y}} \cdot \boldsymbol{\nabla} \times \Delta U = \hat{\boldsymbol{e}}_{\boldsymbol{y}} \cdot \boldsymbol{\nabla} \times \Delta \boldsymbol{\nabla} \times \psi \hat{\boldsymbol{e}}_{\boldsymbol{y}} = -\Delta^2 \psi$$

 $\partial_t \Delta \psi - \hat{\boldsymbol{e}}_{\boldsymbol{y}} \cdot \boldsymbol{\nabla} \times (\boldsymbol{U} \cdot \boldsymbol{\nabla}) \boldsymbol{U} = Pr[\partial_x T + \Delta^2 \psi]$

$$\boldsymbol{\nabla} \times \boldsymbol{\nabla} \times f = \boldsymbol{\nabla} \boldsymbol{\nabla} \cdot f - \Delta f$$

$\hat{\boldsymbol{e}}_{\boldsymbol{y}} \cdot \boldsymbol{\nabla} \times (U \cdot \boldsymbol{\nabla}) U = \partial_z (U \cdot \boldsymbol{\nabla}) u - \partial_x (U \cdot \boldsymbol{\nabla}) w$

$$= \partial_{z}(u\partial_{x}u + w\partial_{z}u) - \partial_{x}(u\partial_{x}w + w\partial_{z}w)$$

$$= \partial_{z}u \partial_{x}u + \partial_{z}w \partial_{z}u - \partial_{x}u \partial_{x}w - \partial_{x}w \partial_{z}w$$

$$+ u \partial_{xz}u + w \partial_{zz}u - u \partial_{xx}w - w \partial_{xz}w$$

$$= \partial_{z}u (\partial_{x}u + \partial_{z}w) - \partial_{x}w (\partial_{x}u + \partial_{z}w)$$

$$+ u \partial_{x}(\partial_{z}u - \partial_{x}w) + w\partial_{z}(\partial_{z}u - \partial_{x}w)$$

$$= (-\partial_{z}\psi)\partial_{x}(-\partial_{zz}\psi - \partial_{xx}\psi)$$

$$+ (\partial_{x}\psi)\partial_{z}(-\partial_{zz}\psi - \partial_{xx}\psi)$$

$$= (\partial_{z}\psi)\partial_{x}(\Delta\psi) - (\partial_{x}\psi)\partial_{z}(\Delta\psi)$$

 $= -J[\psi, \Delta \psi]$

 $\partial_t \Delta \psi + J[\psi, \Delta \psi] = Pr[\partial_x T + \Delta^2 \psi]$

Linear stability analysis

Linearized equations:

$$\partial_t \Delta \psi = Pr[\partial_x T + \Delta^2 \psi]$$

$$\partial_t T = Ra \ \partial_x \psi + \Delta T$$

Solutions:

$$\begin{split} \psi(x, z, t) &= \hat{\psi} \sin qx \, \sin k\pi z \, e^{\lambda t} \quad q \in \mathcal{R}, \ k \in \mathcal{Z}^+, \ \lambda \in \mathcal{C} \\ T(x, z, t) &= \hat{T} \, \cos qx \, \sin k\pi z \, e^{\lambda t} \\ \uparrow &\uparrow \\ \text{functions} \quad \text{scalars} \quad \gamma^2 \equiv q^2 + (k\pi)^2 \end{split}$$

$$\begin{aligned} -\lambda \gamma^2 \hat{\psi} &= Pr[-q\hat{T} + \gamma^4 \hat{\psi}] \\ \lambda \hat{T} &= Ra \ q \ \hat{\psi} - \gamma^2 \hat{T} \end{aligned}$$

$$\lambda \begin{bmatrix} \hat{\psi} \\ \hat{T} \end{bmatrix} = \begin{bmatrix} -Pr \ \gamma^2 \ Pr \ q/\gamma^2 \\ Ra \ q \ -\gamma^2 \end{bmatrix} \begin{bmatrix} \hat{\psi} \\ \hat{T} \end{bmatrix}$$

Seek: $\lambda = 0$ $Pr \ \gamma^4 - Pr \ Ra \ \frac{q^2}{\gamma^2} = 0$ $Ra = \frac{\gamma^6}{q^2} = \frac{(q^2 + (k\pi)^2)^3}{q^2} \equiv Ra_c(q, k)$

Convection Threshold



Conductive state unstable at (q, k) for $Ra > Ra_c(q, k)$

Conductive state stable if

$$\begin{array}{c} \min \\ Ra < \quad q \in \mathcal{R} \\ k \in \mathcal{Z}^+ \end{array} Ra_c(q,k)$$

$$0 = \frac{\partial Ra_c(q,k)}{\partial q} = \frac{q^2 3 (q^2 + (k\pi)^2)^2 2q - 2q(q^2 + (k\pi)^2)^3}{q^4}$$
$$= \frac{2(q^2 + (k\pi)^2)^2}{q^3} (3q^2 - (q^2 + (k\pi)^2))$$
$$\implies q^2 = \frac{(k\pi)^2}{2}$$

$$Ra_{c}\left(q = \frac{k\pi}{\sqrt{2}}, k\right) = \frac{(k\pi)^{2}/2 + (k\pi)^{2}}{(k\pi)^{2}/2} = \frac{27}{4}(k\pi)^{4}$$
$$Ra_{c} \equiv Ra_{c}\left(q = \frac{\pi}{\sqrt{2}}, k = 1\right) = \frac{27}{4}(\pi)^{4} = 657.5$$

Rigid Boundaries



Calculation follows the same principle, but more complicated. Boundaries damp perturbations \implies higher threshold

 $q_c \downarrow \Longrightarrow \ell_c = \pi/q_c \uparrow \Longrightarrow \text{rolls} \approx \text{circular}$

	Ra_c	q_c	ℓ_c
stress-free boundaries	$\frac{27}{4}\pi^4 = 657.5$	$\frac{\pi}{\sqrt{2}}$	1.4
rigid boundaries	≈ 1700	$\approx \pi$	≈ 1

Instabilities of straight rolls: "Busse balloon"





skew-varicose instability

cross-roll instability

Continuum-type stability balloon in oscillated granulated layers, J. de Bruyn, C. Bizon, M.D. Shattuck, D. Goldman, J.B. Swift & H.L. Swinney, Phys. Rev. Lett. 1998.

Complex spatial patterns in convection



Experimental spiral defect chaos Egolf, Melnikov, Pesche, Ecke Nature **404** (2000)



Spherical harmonic $\ell = 28$ P. Matthews Phys. Rev. E. **67** (2003)



Convection in cylindrical geometry. Bajaj et al. J. Stat. Mech. (2006)

Geophysics

Convection and plate tectonics Thermal convection, constant viscosity -500 -1000 (Ey) N −1500 -2000 -2500 0 1000 2000 3000 4000 5000 6000 7000 8000 x (km)

Numerical simulation of convection in earth's mantle, showing plumes and thin boundary layers. By H. Schmeling, Wikimedia Commons.

Convection cells in the sun



ESO Press Phote 29/07 (6 July 2007)

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COUPTOSS FIND 2000 (0 JUSY 2007)



Latitudinal circulation \implies Hadley cell, mid-latitude cell, polar cell

Solutal Convection

Mixture of two species whose density depends on the relative concentration:

$$\rho(C) = \rho_0 \left[1 - \beta(C - C_0) \right]$$

Impose concentration C_0 below and C_1 above. Base state has uniform concentration gradient C^* . Define deviation \hat{C} from base state C^* :

$$C^* = C_0 - (C_0 - C_1)\frac{z}{d}$$
 $C = C^* + \hat{C}$

Governing equations

$$\rho_0 \left[\partial_t + (U \cdot \nabla) \right] U = -\nabla \hat{P} + g \rho_0 \beta \hat{C} \hat{\boldsymbol{e}}_{\boldsymbol{z}} + \mu \Delta U$$
$$\nabla \cdot U = 0$$
$$\left[\partial_t + (U \cdot \nabla) \right] \hat{C} = \frac{C_0 - C_1}{d} U \cdot \hat{\boldsymbol{e}}_{\boldsymbol{z}} + \kappa_C \Delta \hat{C}$$

lead to solutal Rayleigh number and Schmidt number:

 $Ra_{C} \equiv \frac{(C_{0} - C_{1})d^{3}g\beta}{\kappa_{C}\nu}$ non-dimensional measure of concentration gradient $Sc \equiv \frac{\nu}{\kappa_{C}}$ momentum diffusivity / mass diffusivity

The convection in the earth's mantle is solutal.

Thermosolutal Convection

$$\rho(T,C) = \rho_0 \left[1 - \alpha(T - T_0) + \beta(C - C_0)\right]$$

$$\overline{\partial_t \Delta \psi + J[\psi, \Delta \psi]} = Pr[\partial_x T + \partial_x C + \Delta^2 \psi$$

$$\partial_t T + J[\psi, T] = Ra \ \partial_x \psi + \Delta T$$

$$\partial_t C + J[\psi, C] = Ra_C \ \partial_x \psi + \frac{Pr}{Sc} \Delta C$$

Linear Stability Analysis: set J[.,.] = 0 and substitute

If thermal and solutal convection oppose each other, λ can be complex \implies time-dependent states, like traveling and standing waves:



Marangoni Convection: Mechanism

Surface tension varies with temperature. Define Marangoni number.

$$\sigma(T) = \sigma_0 [1 + \gamma (T - T_0)] \qquad Ma \equiv \frac{(T_0 - T_1) d\sigma_0 \gamma}{\kappa \mu}$$

Marangoni boundary condition at upper surface:

1

$$\frac{\partial u}{\partial z} = -\frac{\partial \sigma}{\partial x} = -\gamma \frac{\partial T}{\partial x}$$
 and $w = 0$

Along free surface, fluid moves towards region with lower surface tension.



Under region with high (low) surface tension, fluid rises (falls).

Marangoni Convection: Pattern

Experimental visualization of Marangoni convection by L. Koschmieder:



Hexagonal cells are formed in Marangoni convection because of asymmetry between top and bottom (theory of dynamical systems and pattern formation).

Marangoni Convection: History

Henri Bénard, "Les tourbillons cellulaires dans une nappe liquide transportant de la chaleur par convection en régime permanent", Annales de Chimie et de Physique, **23** 62–144 (1901).

Bénard (1901) and Rayleigh (1916) thought that the motion was due to $\rho(T)$. Block (1956) and Pearson (1958) showed that Bénard's cells were due to $\sigma(T)$. Bénard's experiment showed hexagonal cells. In fact, buoyancy-driven ($\rho(T)$) convection usually forms rolls, not hexagons. But we still call buoyancy-driven convection "Rayleigh-Bénard convection", even though Bénard did not see it.

